Delete, in its entirety, Table 13 on page 49 of the specification as filed and insert, in its place the following replacement Table 13 with the changes indicated at Exhibit Tab A:

Table 13

CONCEN-TRATION OF PEG (%)	pH	% POLYMER IN THE STARTING IVIG SOLUTION	CONCEN-TRATION OF SORBITOL (%)	PRESENCE OF PRECI-PITATE (1)	(%) RECOVERY OF PROTEIN IN THE FILTRATE (2)
3.0	8.0	n.d.	0.4	YES (+++)	N.R.
3.0	8.0	n.d.	5	YES (+)	N.R.
3.0	8.0	n.d.	10	NO (-)	N.R.
3.0	8.0	3.97	9.4	YES (+++)	83.6
3.0	8.0	3.97	13.0	YES (+++)	92.2

IN THE CLAIMS:

Amend claims 20, 24, 42 and 44-46 as indicated on the attached Exhibit A, so that the claims read as follows:

20. (Once amended) A method for the production of virus-inactivated human gammaglobulin G according to claim 19 in which the filtered effluent is pasteurized in the presence of a sugar-alcohol.

24. (Once amended) A method for the production of virus-inactivated human gammaglobulin G according to claim 23 in which, before said treatment with solvent/detergent, the pasteurised effluent is diluted with water for injection so that:

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(a) the concentration of sugar alcohol is 25% (w/w) or less, and

(b) the concentration of protein is between 1% and 3% (w/v).

42. (Once amended) A method for the production of virus-inactivated human gammaglobulin G according to claim 35, further comprising steps of:

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(a) adding an alkali to the acid solution so that the pH is adjusted to between 7.5 and 8.5, and

(b) precipitating and separating insoluble high molecular weight aggregates from the pH adjusted solution.

44. (Once amended) A method for the production of virus-inactivated human gammaglobulin G according to claim 42 further comprising, after separating insoluble high molecular weight aggregates from the pH adjusted solution, diafiltration and concentration of the solution, pH adjusted to 4.0 - 4.8, through ultrafiltration membranes of 100 kDa nominal molecular cut-off and at a transmembrane pressure below 1.2 bar.

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